



FACULTY
OF MECHANICAL
ENGINEERING
CTU IN PRAGUE



DEPARTMENT OF
ENVIRONMENTAL
ENGINEERING

Ventilation / „Fun Vent“

10. Duct design

Bachelor / Master degree course

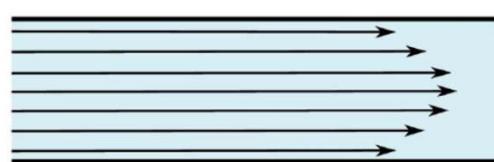
Vladimír Zmrhal

4/2022

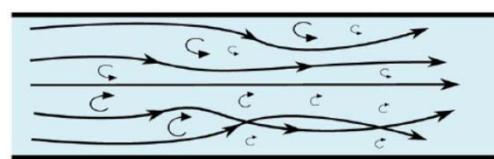
■ Laminar and turbulent flows



laminar flow



turbulent flow



Laminar and turbulent flows



Reynolds number (in circular duct)

$$Re = \frac{wd}{\nu}$$

- laminar flow $Re \leq 2300$
- transitional flow $2300 < Re < 10000$
- fully turbulent flow $Re > 10000$

ν_{air} ... kinematic viscosity [m^2/s] = 14.5×10^{-6} [m^2/s]

3

Laminar and turbulent flows



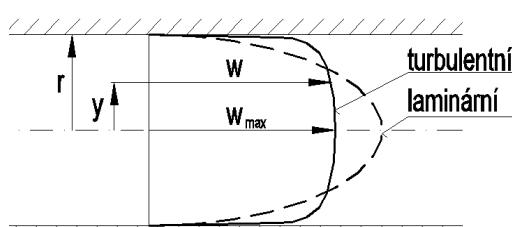
Flow characteristics

$$\frac{w}{w_{max}} = \left(1 - \frac{y}{r}\right)^{1/n}$$

$$V = w_s S$$

$$w_s = \frac{1}{\pi r^2} \int_S w dS$$

$$w_s = \frac{1}{\pi r^2} \int_S w_{max} \left(1 - \frac{y}{r}\right)^{1/n} 2\pi y dy$$



n ... exponent $f(Re)$

$$\frac{w_s}{w_{max}} = 0,817$$

4

■ Pressure losses



Bernoulli equation

$$p_{s1} + h_1 \rho g + \frac{\rho}{2} w_1^2 = p_{s2} + h_2 \rho g + \frac{\rho}{2} w_2^2 + \Delta p$$

Pressures in the duct

$$p = p_s + p_d = p_s + \frac{w^2}{2} \rho$$

$$\Delta p = \left(p_{s1} + \frac{\rho}{2} w_1^2 \right) - \left(p_{s2} + \frac{\rho}{2} w_2^2 \right) = p_{l1} - p_{l2}$$

5

■ Pressure losses



- friction
- local pressure losses

$$\Delta p = \underbrace{\lambda \frac{l}{d} \frac{w^2}{2} \rho}_{\text{friction}} + \underbrace{\sum \zeta \frac{w^2}{2} \rho}_{\text{local losses}} = R.l + Z \quad w = \frac{\dot{V}}{A} = \frac{4\dot{V}}{\pi d^2}$$

$$\Delta p = \left(\lambda \frac{l}{d} + \sum \zeta \right) \frac{w^2}{2} \rho = k \dot{V}^2$$

$$k = \left(\frac{\lambda \cdot l}{d} + \sum \zeta \right) \frac{8 \cdot \rho}{\pi^2 \cdot d^4}$$

6

■ Friction losses



Laminar flow

$$\lambda = \frac{64}{Re}$$

Turbulent flow

$$\frac{1}{\sqrt{\lambda}} = -2 \log \left(\frac{\varepsilon / d}{3.71} + \frac{2.51}{Re \sqrt{\lambda}} \right)$$

Note:

Darcy-Weisbach λ
Fanning friction factor f

$$\lambda = 4f$$

Colebrook (1939)
 ε/d – relative roughness

$$\lambda = \frac{0.0812}{Re^{0.125} d^{0.11}}$$

Smolik (1959) for $\varepsilon = 0.15$

7

■ Friction losses



Turbulent flow

$$\lambda = \frac{0.3164}{\sqrt[4]{Re}}$$

for smooth pipes and duct (plastic)
 $5000 < Re < 80\,000$

8

■ Friction losses



Roughness height of the conduit wall surfaces

Material	ϵ (mm)
Galvanized steel	0.15
Concrete duct – smooth surface	0.5
Concrete duct – rough surface	1.0 – 3.0
Smooth brass, copper	0.015
Hose pipe	0.6 - 3
Plastic pipe	0.007

9

■ Friction losses



Hydraulic diameter

$$d_h = \frac{4A}{O} = \frac{4ab}{2(a+b)} = \frac{2ab}{a+b}$$

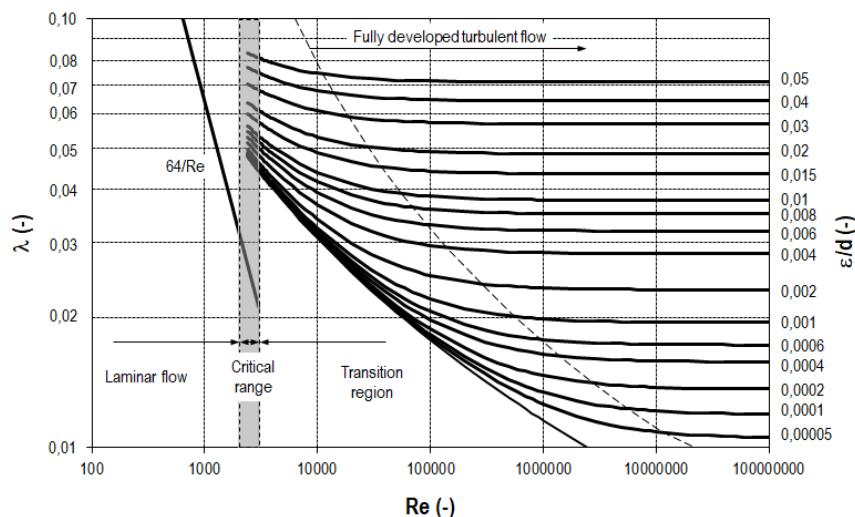
Rectangular ducts - correction

$$\lambda = C\lambda_d$$

$$C = 1.1 - 0.1 \frac{b}{a}$$

10

■ Moody chart



11

■ Local pressure losses



Local pressure losses are caused by the fluid flow through the duct fittings:

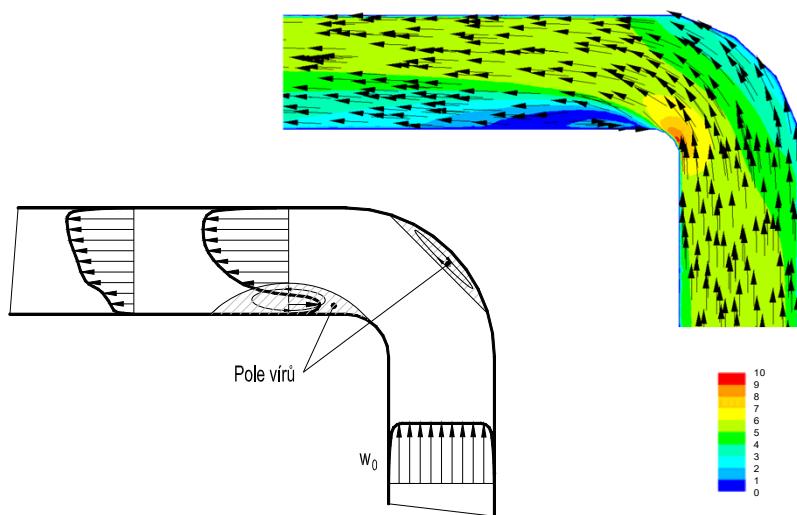
- which change the direction of the flow (**elbows, bands, etc.**)
- affect the flow in the straight duct with constant cross-section (**valves, stopcocks, filters etc.**).

$$\Delta p_l = \sum \zeta p_d = \sum \zeta \frac{w^2}{2} \rho$$

- ζ ... local loss coefficient (experiments - see Idelchik 1986)
- experimental data (except Borda loss)

12

■ Local pressure losses

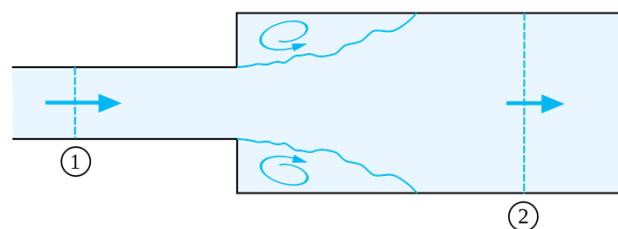


13

■ Borda loss



Flow expansion



Borda – Carnot eq.

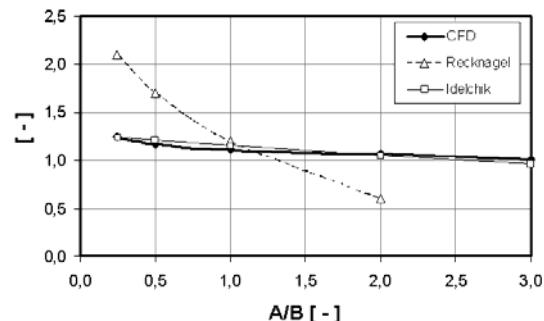
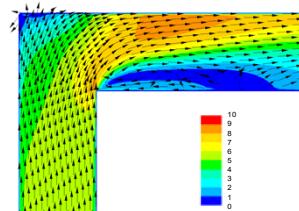
$$\Delta p_l = \left(\frac{A_2}{A_1} - 1 \right)^2 \frac{w_2^2}{2} \rho$$

14

■ Local pressure losses - example



$$\zeta = 1.11 \left(\frac{a}{b} \right)^{-0.08}$$



15

■ Duct design



Methods

- velocity method
- equal-friction method
- static regain method

16

■ Velocity method



Duct design procedure:

- 1) Find the **main line**

Rule no. 1: the main line is the maximum pressure loss line
(longest line, most segment line (?))

- 2) Air flow rate **$V(m^3/h)$** in duct sections is known

- 3) **Selection** of the air velocity in the duct **w**

Rule no. 2: Air velocity increase towards the fan

17

■ Velocity method



	Air velocity w (m/s)			
	Main section	Side section		
Ventilation and low-pressure air-conditioning	recomend.	max.	recomend.	max.
- residential buildings	3.5 - 5	6	3	5
- public buildings	5 - 7	8	3 - 4.5	6.5
- industry	6 - 9	11	4 - 5	9
High-pressure air-conditioning	8 - 12	15 - 20	8 - 10	18

18

■ Velocity method



4) duct area A (m^2) → diameter d or $a \times b$

$$d = \sqrt{\frac{4V}{\pi w}}$$

→ nominal diameter d_N or $a_N \times b_N$

Rule no. 3: Duct sizes: 80, 100, 125, 140, 160, 180, 200, 250, 315, 355, 400, 450, 500, 560, 630, 710, 800, 900, 1000, 1120, 1250, 1400, 1600, 1800, 2000

19

■ Velocity method



5) $d_N \rightarrow$ real velocity w_{real}

$$w_{real} = \frac{4V}{\pi d_N^2}$$

6) calculation of dynamic pressure p_d

7) Reynolds number → friction coefficient λ

8) local loss coefficients ζ

9) pressure loss of the duct section $\Delta p_{z,i}$

$$\Delta p_i = \left(\lambda \frac{l_i}{d_i} + \sum \zeta \right) \frac{w_i^2}{2} \rho$$

20

■ Velocity method



Rule no. 4: Balancing

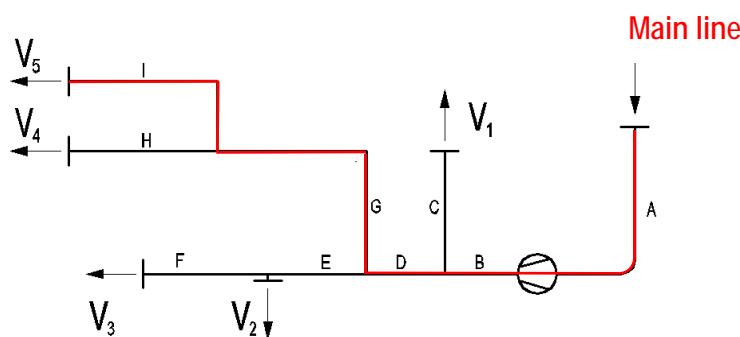
$$\Delta p_F + \Delta p_E = \Delta p_G + \Delta p_I$$

- 10) total pressure loss is the sum of the duct sections pressure losses

$$\Delta p = \sum \Delta p_i$$

21

■ Velocity method

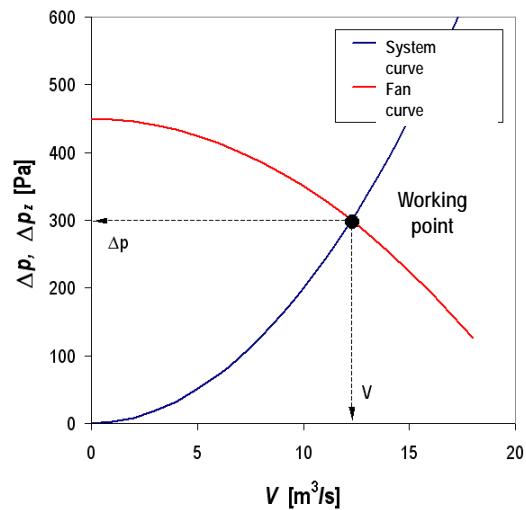


$$\Delta p = \Delta p_A + \Delta p_B + \Delta p_D + \Delta p_G + \Delta p_I$$

$$\dot{V} = \dot{V}_1 + \dot{V}_2 + \dot{V}_3 + \dot{V}_4 + \dot{V}_5$$

22

■ System and fan curve



23

■ Example



Example 1: Dimension the air duct system. Use the velocity method.

air velocity $w = 6 - 10 \text{ m/s}$,

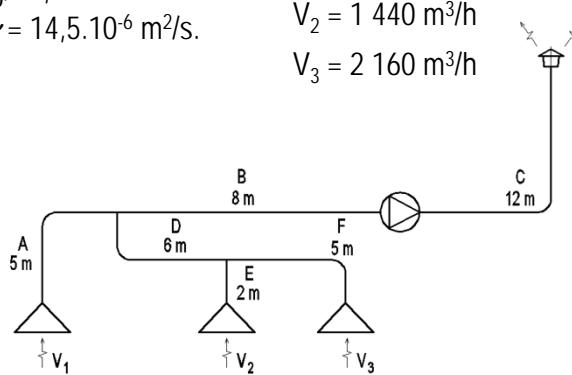
$$V_1 = 9000 \text{ m}^3/\text{h}$$

air density $\rho = 1.2 \text{ kg/m}^3$,

$$V_2 = 1440 \text{ m}^3/\text{h}$$

kinematic viscosity $\nu = 14.5 \cdot 10^{-6} \text{ m}^2/\text{s}$.

$$V_3 = 2160 \text{ m}^3/\text{h}$$



24

■ Example



Example 1:

$$D_{calc} = \sqrt{\frac{4V}{\pi w}} \quad \Rightarrow \quad D_N \quad \Rightarrow \quad w_{real} = \frac{4V}{\pi D_N^2}$$

$$\Rightarrow \quad Re = \frac{w_{real} D_N}{\nu} \quad \Rightarrow \quad \lambda = \frac{0,0812}{Re^{0,125} D_N^{0,11}}$$

$$\Delta p_f = \lambda \frac{l}{D} \frac{w_{real}^2}{2} \rho \quad \Delta p_l = \sum \zeta \frac{w_{real}^2}{2} \rho$$

$$\Delta p_{l,i} = \Delta p_f + \Delta p_l (+\Delta p_{el})$$

25

■ Example



Line	I	V	V	w _{calc}	D _{calc}	D _N	w _{real}	p _d	Re	I	Δp _f	Σζ	Δp _l	Δp _{el}	Δp _t
-	m	m ³ /h	m ³ /s	m/s	mm	mm	m/s	Pa	-	-	Pa	-	Pa	Pa	Pa
											0,41		19		
											0,96		0		
											0,46		0		
											2,04		0		
TOTAL															XX

26

■ Equal-Friction Method



Duct design procedure:

- 1) selection of pressure loss per unit length $R = 0,8 - 4 \text{ Pa/m}$

$$R = \lambda \frac{1}{d} \frac{w^2}{2} \rho$$

- 2) local pressure losses \rightarrow friction in straight duct with equivalent length

$$\lambda \frac{l_e}{d} \frac{w^2}{2} \rho = \zeta \frac{w^2}{2} \rho \Rightarrow l_e = \frac{\zeta}{\lambda} d$$

- 3) duct section pressure loss

$$\Delta p = R(l + l_e)$$

27

■ Equal-Friction Method



Friction chart

Choice:

$$R = 1 \text{ Pa/m}$$

Air flow rate:

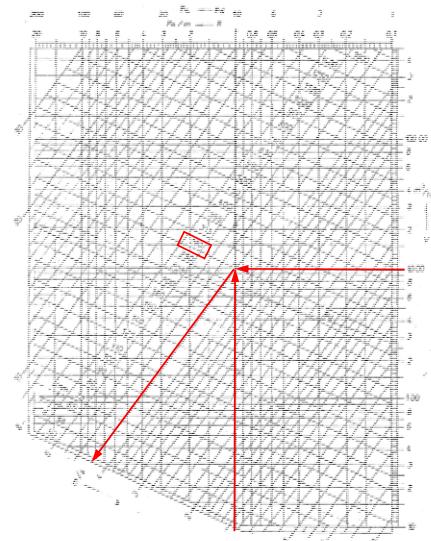
$$1000 \text{ m}^3/\text{h}$$

diameter D:

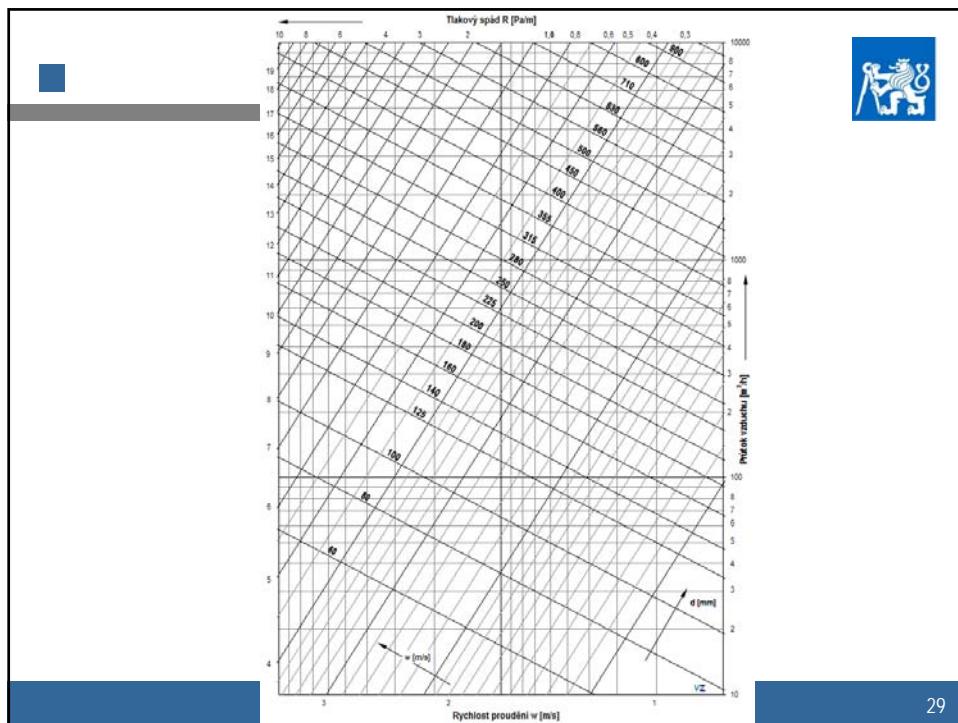
$$280 \text{ mm}$$

Velocity :

$$w = 4,5 \text{ m/s}$$



28



29

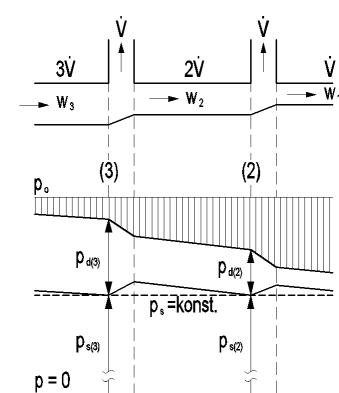
■ Static Regain Method



- for uniform air supply
- constant static pressure before the branch

Principle

- cross section reduction after branches to change the dynamic pressure
- decreasing of dynamic pressure balances the pressure losses in the duct section



$$\Delta p_{z3-2} = p_{d3} - p_{d2}$$

30

■ Static Regain Method



Assumptions:

- $V_i = \text{const.}$
- $b = \text{const.}$
- $i = n, n-1, \dots, 1$
- calculation of dimension a

$$a_{i-1} = a_i \sqrt{1 + \frac{\lambda_{i-1}}{d_{i-1}} l_{i-1}} \frac{i-1}{i}$$

31

■ Static Regain Method



Deduction:

$$\Delta p_{z2-1} = p_{d2} - p_{d1}$$

$$\lambda \frac{l_1}{d_1} \frac{w_1^2}{2} \rho = \frac{w_2^2}{2} \rho - \frac{w_1^2}{2} \rho \quad \text{kde} \quad w_1 = \frac{\dot{V}_1}{a_1 b}, w_2 = \frac{\dot{V}_2}{a_2 b}$$

$$\lambda \frac{l_1}{d_1} \frac{\dot{V}_1^2}{a_1^2 b^2} = \frac{\dot{V}_2^2}{a_2^2 b^2} - \frac{\dot{V}_1^2}{a_1^2 b^2}$$

32

■ Static Regain Method



⇒

$$\lambda \frac{l_1}{d_1} \frac{\dot{V}_1^2}{a_1^2} = \frac{\dot{V}_2^2}{a_2^2} - \frac{\dot{V}_1^2}{a_1^2} \quad \leftarrow \quad \dot{V}_1 = \dot{V}, \dot{V}_2 = 2\dot{V}$$

$$\lambda \frac{l_1}{d_1} \frac{1^2 \cdot \dot{V}^2}{a_1^2} + \frac{1^2 \cdot \dot{V}^2}{a_1^2} = \frac{2^2 \cdot \dot{V}^2}{a_2^2} \Rightarrow \lambda \frac{l_{i-1}}{d_{i-1}} \frac{(i-1)^2}{a_{i-1}^2} + \frac{(i-1)^2}{a_{i-1}^2} = \frac{i^2}{a_i^2}$$

$$a_i^2 \left(1 + \lambda \frac{l_{i-1}}{d_{i-1}} \right) (i-1)^2 = a_{i-1}^2 i^2 \Rightarrow a_{i-1} = a_i \sqrt{1 + \frac{\lambda_{i-1}}{d_{i-1}} l_{i-1}} \frac{i-1}{i}$$

33

■ Duct systems



Shapes

- rectangular
- round
- flexible duct



Materials

- steel galvanized
- aluminium
- plastic PVC
- textile
- ALP



34

■ Duct systems



Duct leakage rate

$$\dot{V} = m \Delta p^{0.67} A_d$$

where A_d ... duct surface [m^2]

Class	Charakteristics of the leakage path $m[\text{m}^3/\text{s per m}^2]$
A	$0.027 \cdot 10^{-3}$
B	$0.009 \cdot 10^{-3}$
C	$0.003 \cdot 10^{-3}$
D	$0.001 \cdot 10^{-3}$

35

■ Thermal insulation



Purpose

- condensation risk
- heat losses/gains

Thickness of TI

- indoor 45 – 60 mm
- outdoor 80 – 100 mm (with sheet covering)

36



Thank you for your
attention



utp.fs.cvut.cz